

On Some of the Properties of Water and of Steam

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III. On some of the Properties of Water and of Steam. By William Ramsay, Ph.D., F.R.S., and Sydney Young, D.Sc.

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[PLATE 7.]

THE work of which an account is given in the following pages was carried out in the winter of 1887-88, and forms a sequel to much of a similar character already published by the authors, on methyl, ethyl, and isopropyl alcohols, on ethyl oxide, on acetic acid, and on a mixture of alcohol and ether ('Phil. Trans.,' 1886, Part I. p. 123; 1887, A., p. 57; 1887, A., p. 313; 1889, A., p. 137; 'Chem. Soc. Trans., 1886, p. 790; 1887, p. 755).

The apparatus with which it was carried out has been fully described in the memoir on ether (loc. cit.). The only important change was in the nature of the glass tubes used to contain the liquid under experiment. While, in the case of the alcohols, ether, &c., lead glass proved the best material for tubes, it is too easily attacked by At comparatively low temperatures it becomes etched, and it is impossible to take readings. Moreover, the water dissolves a not inconsiderable quantity of potassium silicate; tubes of green boiler-gauge glass were, therefore, substituted for tubes of lead glass. This glass consists of a silicate of calcium and potassium, containing a trace of ferrous iron (SiO₂=71·20; CaO=14·99; $K_2O=13·19$; Total, 99·38.) They withstand a higher pressure than lead-glass tubes, and they are attacked with difficulty. Even after an exposure of several days to liquid water at 280° C., only 0.7 per cent. of residue remained on evaporating the water. Inasmuch as some of the material of the glass is dissolved, however, the water cannot be considered to be absolutely pure, but the results may be given as the best attainable with water in contact with glass.

It may be advisable to state here again, that the *pressures* were read from gauges containing dry air, kept at a known temperature by jackets of running water; and that they are corrected for deviation from Boyle's law by help of experiments made by Amagat ('Compt. Rend.,' vol. 99, p. 1153); that the temperatures are those of an air-thermometer, and that they were secured by jacketing the tube containing the water with the vapours of pure chlorobenzene, bromobenzene, aniline, methyl-salicylate, or bromonaphthalene, of which the vapour-pressures corresponding to known temperaDRS. W. RAMSAY AND S. YOUNG ON SOME OF

tures have been determined by us ('Chem. Soc. Trans.,' vol. 47, p. 640). By causing one or other of these liquids to boil under definite known pressures, any desired temperature, within certain limits, was attainable; and, as a small alteration of temperature corresponds to a considerable alteration of pressure, it may be taken for certain that the temperatures are practically correct. The expansion of the glass made use of for the volume tube was carefully determined, and a correction was in all cases applied, so that the apparent volumes are reduced to real volumes. tion, however, was applied for the alteration in the volume tube due to internal pressure, because an estimation of its amount showed it to be much within the error of reading volume.

The results may be classified under three heads:—

- I. Expansion of liquid water.
- II. Vapour-pressures.
- III Density of unsaturated and saturated steam.

I. Expansion of Liquid Water.

For these experiments, the tube was two-thirds filled with water freed from air by That no air was present was often proved during the experiments by condensing a bubble of steam; condensation always took place without appreciable rise of pressure. The weight of water taken was deduced from observations of its volume at the ordinary temperature, both before and after experiment. are as follows:—

Temperature.	Divisions of tube.	Volume at 4 and weight.
$\begin{cases} 12.25 \\ 12.40 \\ 15.7 \\ 17.9 \end{cases}$	$\begin{array}{c} 246.75 \\ 246.90 \\ 246.20 \\ 246.25 \end{array}$	c.c. or grm. 1·1054 1·1060 1·1031 1·1035

The first pair of readings was taken before the commencement of the experiments; the second pair after the expansions had been measured. The small difference is probably due to adherence of liquid to the lower portions of the tube, which had become etched during the experiments.

The mean result, from which the following Table is calculated, is 1:1045 c.c. at 4°, or 1.1045 grm :—

THE PROPERTIES OF WATER AND OF STEAM.

m	Volume of 1	grm. in c.cs.	m	Volume of 1	grm. in c.cs.
Temperature.	Observed.	Smoothed.	Temperature.	Observed.	Smoothed.
100 110 120 130 140 150 160 170 180	1·0432 1·0510 1·0594 1·0678 1·0791 1·0880 1·0996 1·1124 1·1260	1.0432 1.0513 1.0592 1.0678 1.0772 1.0878 1.0995 1.1124 1.1260	200 210 220 230 240 250 260 270	1·1412 1·1567 1·1734 1·1915 1·2122 1·2319 1·2516 1·2750 1·3000	1.1407 1.1566 1.1733 1.1914 1.2112 1.2320 1.2533 1.2755 1.2985

Note.—The pressures are here nearly those of the vapour at the respective temperatures.

The volumes of 1 grm. of water have been measured by Mendeléeff ('Liebig's Annalen, vol. 119, 1861, p. 10), and by HIRN ('Annales de Chimie' [4], vol. 10, 1866, p. 32). The following short Table shows that HIRN's results agree very closely with those given by us:-

T. C.		Volume of 1 grm	
Temperature.	Mendeléeff.	Hirn.	R. and Y.
100 120 131 140 156·8 160 180 200	1·0428 1·0722 1·1016 	1 04315 1 05992 1 07949 1 10149 1 12678 1 15900	1·0432 1·0594 1·0791 1·0996 1·1260 1·1567

The compressibility of water was measured at 190° and at higher temperatures. The results are as follows:—

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Temperature.	Volume of 1 grm.	Pressures of mercury.	Temperature.	Volume of 1 grm.	Pressures of mercury.
190	cub. centims. 1:1412 1:1408 1:1386	millims. 9,837 12,813 30,029	2 [°] 30	cub. centims. 1·2122 1·2101 1·2079	millims. 21,085 31,745 42,249
200	1.1365 1.1567 1.1559 1.1538	39,904 15,014 18,695 30,513	240	1·2319 1·2300 1·2282	25,276 32,452 41,614
210	1·1516 1·1734 1·1732 1·1710	43,901 14,404 17,488 31,467	250 260	1.2516 1.2508 1.2490 1.2750	30,059 36,040 43,925 35,028
220	1·1689 1·1915 1·1905 1·1884	43,405 17,622 27,251 39,432		1.2735	40,210

II. Vapour-pressures.

The pressures of the vapour were read from experiments with a larger quantity of water in the tube, as well as when the quantity was small; but uniform results were not obtained. The vapour-pressure of water, unlike that of other liquids, depends to some extent on the amount of substance present.* This is to be attributed to the fact, that with only a small amount of liquid present, a relatively large surface of the tube is exposed to the vapour, and, as there can be no doubt that the vapour adheres to the surface, the pressure is lowered to a certain extent. The results, with the larger quantity, are therefore given as probably more correct. Each pressure is the mean of some seven or eight readings in which the relative volumes of water and steam were altered within the greatest limits which the tube allowed.

The pressures are, as before stated, corrected for deviations from Boyle's law.

To facilitate comparison, the results obtained by Regnault and others are placed in juxtaposition with ours; and also columns showing the differences between our results and those obtained in other ways. The columns are distinguished as follows:--

- "R. and Y." stands for RAMSAY and Young.
- "Reg. curve" stands for Regnault's copper-plate curves, given in the 'Mémoires de l'Académie, vol. 26.
- "Reg. H." and "Reg. F." signify Regnault's results calculated by Biot's formula, $\log p = a + b\alpha^t + c\beta^t$, using the constants marked H and F respectively.
 - "Reg K." signifies Regnault's formula K, viz., $p = a \alpha^{x/(1+mx)}$
 - * See Appendix, pp. 120 and 121.

"Unwin" ('Phil. Mag.,' 1886, p. 299). His formula is $\log p = 7.5030^{-7.579/l^{1-25}}$.

"Antoine" refers to the last formula given by Ch. Antoine ('Annales de Chimie,' 1891, vol. 22,' p. 283). It is $\log p = 7.921^{-1638/t + 225}$. It has the merit of allowing temperature to be calculated from pressure, as easily as the converse; the results, however, calculated in each way, are not absolutely the same, but do not differ to any important extent.

"Buff" ('Liebig's Annalen,' Suppl. 2, 1862-3, p. 137) uses the formula

$$\log p = \log \frac{760}{373} + \log (273 + t) + \frac{\log (273 + t) - \log 373}{\alpha}.$$

$$\alpha = 0.06479 + 0.0001722 t - 0.0000001 t^{2}.$$

RANKINE" ('Steam Engine,' 9th Ed., p. 237) gives the formula

$$\log p = A + \frac{B}{\tau} + \frac{C}{\tau^2}.$$

'Broch" ('Travaux et Mémoires du Bureau Internat. des Poids et Mesures,' vol. 1, p. 19, et seq.). His formula is

$$p = a.10 \frac{bt + ct^2 + dt^3 + et^4 + ft^5}{1 + \alpha t}.$$

M. Broch has undertaken a most laborious investigation of the formulæ employed for the calculation of the vapour-pressures of water, adopting finally the one given in the table. The utmost care was taken to obtain the best possible results from the data taken; but, unfortunately, M. Broch has accepted Regnault's conclusion that the curve representing the vapour-pressures of ice is continuous with that obtained from the vapour-pressures of water, and he has employed the whole of the data from -32° to 100° . By the method of calculation of the constants for the formula, this source of error has been to a certain extent eliminated, as is shown by the comparison (p. 31) of Regnault's individual observations with the pressures calculated from the formula. In this table it is seen that below -5° , out of 31 comparisons, the calculated pressures are higher than those observed in every case but one. The error is, however, only partially eliminated, and this probably explains the fact that the formula, with the constants given, will not bear extrapolation above 100° even to 120° , though it is supposed to hold good through a range of 132° .

It is to be feared that the results between 0° and 100° may even be to some extent vitiated by this source of error—a most unfortunate circumstance, considering the enormous amount of labour bestowed on the work, and the fact that the pressures calculated from the formula have received the *imprimatur* of the Bureau International.

It is to be noticed that REGNAULT'S formula K gives results nearest the truth, but that fairly approximate results are also obtainable by the use of Unwin's and of Antoine's formulæ. These formulæ, it need hardly be remarked, are all empirical.

Table of Vapour-pressures of Water.

T.	T. R. & Y.	Reg. Curve.	٦	Reg. H.	Δ22	Reg. F.	Δ3	Reg. K.	₫	Unwin.	δ	An- TOINE.	Δ_6	BUFF.	Δ_7	RAN- KINE.	\$	Broch.	จ์	
120	1,484	1	1,489 + 5	1,491 +	+ 7	1,491	1 +	1,487	+ 3	1,486	+	1,491	+	1,491	+ 4	1,491	2 +	1,545	+	61
130	2,019		10	2,030	П	2,030	11	2,023	4	2,020		2,030	П	2,029	10	2,030	11			
140	2,694		19	2,718	24	2,718	24	2,706	12	2,710	16	2,718	24	2,716	55	2,716	22			
150	3,568	3,572	4	3,581	13	3,582	14	3,564 -	4	3,564	4	3,581	13	3,578	10	3,578	10	4,244	+	929
160	4,652	4,647	ا ت	4,652	0	4,652	0	4,629	-23	4,633	- 19	4,652	0	4,646	9 -	4,647	ا س			
170	5,937	5,960 + 21	+21	5,962	25	5,959	22	5,933	4 -	5,942	+· 30	5,962	25	5,953	+ 16	5,955	+ 18			make managember
180	7,487	7,545	49	7,546	89	7,537	59	7,513	+35	7,525	47	7,546	89	7,535	52	7,539	61			
190		9,428	25	9,443	40	9,425	22	9,407	4	9,423	20	9,443	40	9,429	56	9,432	53			
500	11,625	11,625 11,660	35	11,689	64	11,663	38	11,656	31	11,665	40	11,689	64	11,672	47	11,679	54	31,861	+20,237	237
210	14,240	210 14,240 14,308	89	14,325	85	14,297	52	14,302	62	14,316	92	14,325	85	14,310	20	14,319	29			
220	17,365	220 17,365 17,390	25	17,390	25	17,381	16	17,390	25	17,398	83	17,390	25	17,386	21	17,390	25			
230	230 20,936	20,915	-21	20,926	- 10	20,981	45	20,965	53	20,952	16	20,926	- 10	20,937	-	20,936	0		-	
240	25,019	•	:	24,973	- 46	25,176	157	25,074	55	25,046	22	25,027	∞ +	24,966	- 53	25,009	- 10			
250	29,734	:	:	29,571	29,571 -163	30,072	338	29,765	31	29,694	- 40	29,689	45	29,687	- 47	29,648	98			at 100
260	260 35,059	:		34,757 -302	-305	35,798	739	35,086	27	34,965	- 94	34,970	68	34,978	- 81	34,898	161			
270	270 41,101	•	•	40,570	40,570 531 42	42,545	1444	41,088 -13	-13	40,887 -214	-214	40,926 -175	-175	40,948 -153	-153	40,794	307			
_			_							\ 		\		>				-		-

* Observed. The details of the observations are to be found in the Appendix, pp. 120 and 121.

III. The Densities of the Saturated and Unsaturated Vapour of Water at Different Temperatures and Pressures.

The method pursued was (1) to find the weight of the small quantity of water in the tube by ascertaining the values of the products of pressure and volume at large volumes and at high temperatures. If these products, for slight decrease of volume, and at any one temperature, were sensibly constant, and if the products at different temperatures bore to one another the same ratio as that between the absolute temperatures, it was assumed that the vapour-density of the steam was normal; if hydrogen be taken as unity, the density is nine. The weight could then be calculated by the equation given in the Appendix, p. 122. (2) The volume of the gas was then diminished by regular decrements at temperatures rising by 10° at a time, and the pressure corresponding to each volume was read. From these data the volume of 1 grm. in cubic centimetres could be calculated. When the volume was sufficiently diminished condensation ensued.

Two distinct sets of experiments were made: one with a large tube at low temperatures, and one with a strong pressure tube at high temperatures. The actual experimental data for high temperatures (120° to 270°) are given on pp. 124–127 of the Appendix; those at low temperatures on pp. 128–130. Reasons are there adduced to show that when the pressure approaches the vapour-pressure condensation on the glass occurs. This causes the pressure to be lower than it should be for a given volume, and renders the results very difficult to interpret. Such adhesion appears to be slight at large volumes where the vapour is unsaturated; but, as it occurs gradually, the effect is that on decreasing volume some water is left below the mercury, and as there is no clue to the amount thus trapped the weight is diminished by an unknown amount. But it is reckoned as undiminished, and hence in calculating the volume of 1 grm. from the actual measurements the volume ascribed is too small, and too small by an unknown quantity. At the same time the pressure is lowered by the adhesion to the glass, and so the curve is distorted as it approaches the pressure of the saturated vapour.

Under the circumstances it appeared best to follow the experimental results as closely as possible. However interesting from a theoretical point of view the absolute expansion of water-gas may be, in practice it is always in contact with a surface; and although it is probable that the material, as well as the extent of the surface, would influence the amount of adhesion, yet an indication of the behaviour of steam in contact with glass cannot fail to be of use in considering the practical case of steam in contact with iron. Moreover, the error is to a great extent eliminated by making use of the volumes of 1 grm. of saturated steam calculated from Regnault's heats of vaporization.

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RANKINE ('Edinb. Trans.,' vol. 23, Part I., 1862, p. 147) discusses the want of concordance between the volumes of saturated steam observed by FAIRBAIRN and TATE, and those calculated from REGNAULT'S observations on the heats of vaporization; and suggests a difference in molecular condition between steam at rest, as in FAIRBAIRN and TATE'S experiments, and in motion, as in REGNAULT'S. scarcely be doubted that the true reason of the discrepancy is to be found in the adhesion of steam to glass. It is obvious that in Regnault's experiments this source of error would be absent, inasmuch as the weight of water was simply that which entered the calorimeter.

Three sets of isothermal curves were drawn in which the experimental numbers were closely followed, the only adjustment being that of rendering the curves as smooth as possible, and of making use of the mutual relations between the curves, so as to smooth out the irregularities of each individual one. These curves were prolonged to the points calculated from Regnault's observations by the formula

$$s_1 = \frac{LJ}{T \frac{dp}{dt}} + s_2,$$

where ε_1 and ε_2 are respectively the volumes of saturated vapour and liquid, L the heat of vaporization, J the mechanical equivalent of heat, T absolute temperature, and dp/dt the differential of pressure in degrees with respect to temperature.

By help of this formula the following table was calculated:—

Vapour-Densities (Saturated) of Water from Regnault's Heats of Vaporization.

THE PROPERTIES OF WATER AND OF STEAM.

t.° C.	T.°abs.	p.	dp/dt.	L (total).	Q.	Ht. of Vap. L.	$s_1 - s_2$.	s_1 .	V.D.
0 10 20 30 40 50 60 70 80 90 100 110	273 283 293 303 313 323 333 343 353 363 373 383	4·600 9·165 17·39 31·55 54·91 91·98 148·8 233·1 354·6 525·4 760·0 1,075		606·5 609·5 612·6 615·7 618·7 621·7 624·8 627·8 630·9 633·9 637·0 640·0	0 10 20 30 40·1 50·1 60·1 70·2 80·3 90·4 100·5 110·6	606·5 599·5 592·6 585·7 578·6 571·6 564·7 557·6 550·6 543·5 536·5 529·4	211,130 108,730 58,867 33,384 19,722 12,078 7,671 5,026 3,386 2,339 1,657 1,191	211,131 108,731 58,868 33,385 19,723 12,079 7,672 5,027 3,387 2,340 1,658 1,192	8·74 8·83 8·89 8·94 8·98 9·04 9·06 9·10 9·13 9·18 9·20 9·29
120 130 140 150 160 170 180 190 200 210 220 230	393 403 413 423 433 443 453 463 473 483 493 503	1,491 2,030 2,718 3,581 4,652 5,962 7,546 9,443 11,689 14,325 17,390 20,926	47.35 60.90 77.06 96.17 118.5 144.1 173.4 206.5 243.4 284.4 329.4 378.5	643·1 646·1 649·2 652·2 655·3 658·3 661·4 664·4 667·5 670·5 673·6 676·6	120·8 131·0 141·2 151·5 161·7 172·1 182·4 192·8 203·2 213·7 224·2 234·7	522·3 515·1 508·0 500·7 493·6 486·2 479·0 471·6 464·3 456·8 449·4 441·9	877·4 656·1 499·0 384·7 300·7 238·1 190·6 154·2 126·1 104·0 86·50 72·54	1,192 878·5 657·2 500·1 385·8 301·8 239·2 191·7 155·3 127·3 105·2 87·70 73·76	9·32 9·32 9·39 9·44 9·52 9·58 9·65 9·73 9·81 9·88 9·96 10·05 10·13

p, Regnault's formula H; dp/dt from same formula; L (total), Q and L from Regnault.

As Regnault's measurements do not extend beyond 230° the higher isothermals were smoothed as well as possible and made to cut the vapour-pressure lines at certain points, to which we were guided to some extent by their own regularity, and to some extent by extending the curve drawn to pass through the points representing the volumes of 1 grm. of saturated vapour. The results cannot be far from the truth.

The next table shown was constructed by reading the pressures and temperatures corresponding to equal volumes.

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-	150°.	160°.	170°.	180°.	190°.	200°.	210°.	220°.	230°.	240°.	250°.	260°.	270°.
	2,190	2,250	2,310	2,370	2,425	2,485	2,540	2,600	2,660	2,720	2,780	2,840	2,900
	2,365	2,425	2,490	2,552	2,615	2,685	2,745	2,810	2,880	2,965	3,015	3,070	3,135
	2,560	2,640	2,710	2,775	2,850	2,925	2,995	3,070	3,145	3,215	3,290	3,350	3,415
	2,810	2,895	2,975	3,045	3,125	3,210	3,295	3,375	3,455	3,535	3,615	3,685	3,760
	3,110	3,205	3,300	3,390	3,475	3,565	3,650	3,740	3,830	3,920	4,010	4,095	4,175
	3,465	3,600	3,705	3,800	3,905	4,000	4,095	4,205	4,305	4,400	4,505	4,600	4,690
	•	4,085	4,215	4,325	4,450	4,560	4,660	4,780	4,905	5,020	£,140	5,260	5,375
	•	•	4,920	5,040	5,170	5,315	5,460	5,595	5,725	5,865	5,995	6,125	6,255
man of the state of the self-state of	•	•	5,760	6,020	6,190	6,360	6,530	6,700	6,870	2,030	7,200	7,360	7,510
hand the Additional Comme	•			7,300	7,660	7,875	8,080	8,300	8,505	8,710	8,930	9,140	9,360
	•				8,580	8,990	9,175	9,430	9,675	006'6	10,120	10,375	10,600
	•	0		•	*	10,230	10,570	10,850	11,100	11,370	11,650	11,930	12,185
	;		•		:	•	12,490	12,860	13,180	13,490	13,840	14,150	14,480
	:	•	•	***************************************	•		•	15,660	16,160	16,545	16,920	17,300	17,700
a haa aa garah kabaas ee a			•		•	•		12,010	17,740	18,180	18,590	19,000	19,400
ATTEMPT OF THE PERSON NAMED IN	:	•		•	•	•	:	:	19,550	20,150	20,650	21,060	21,520
	:	. •	:	THE STATE SALES	•	•	:	•	•	22,470	23,340	23,750	24,200
	•	:		•	:	:	•	•	•	•	26,350	27,060	27,650
· manufacture of the control of	•	•	•	•	:	:	:	•	:	•	•	31,120	32,000
	:	•	:	•	:	:	•	•	•	•	:	33,650	34,780

The vapour-densities and volumes of a gramme of saturated vapour can be given at temperatures above 230°. They are as follows:—

Temperature.	Pressure.	Vol. of 1 grm.	Vapour-den	sity $(H = 1)$.	Vol. of 1 grm.
230 240 250 260 270	millims. 20936 25019 29734 35059 41100	c.c. 73·00 60·65 50·30 42·40 37·20	read. 10·23 10·51 10·87 11·14 11·04	$\begin{array}{c} \text{smoothed.} \\ 10 \cdot 22 \\ 10 \cdot 40 \\ 10 \cdot 63 \\ 10 \cdot 94 \\ 11 \cdot 36 \end{array}$	recalculated. 73.06 61.28 51.43 43.19 36.15

There is very great difficulty in reconciling the results given by REGNAULT at the highest temperatures with our own direct measurements. Regnault's results interpreted as vapour-density obviously increase at too slow a rate above 210°, while ours appear to increase too rapidly at 240°, 250°, and 260°. We therefore constructed a curve showing the relationship of vapour-densities from all sources to temperature; the numbers given as "smoothed" are read from the curve, and the volumes of 1 grm. were again calculated.

In a series of papers published in the 'Philosophical Magazine' (1887, vol. 27, pp. 196 and 435), we showed that for ether, ethyl alcohol, and carbon dioxide, the pressures of the vapours of these substances for constant volumes are, within limits of experimental error, a rectilinear function of the temperature, or p = bt - a, where a and b are two constants, depending on the volume, and t is the absolute temperature. CARL BARUS, as the result of experiments with other substances, has confirmed the statement, both for liquid and gas. He states ('Phil. Mag.,' 1890, vol. 30, p. 358) that "below 1000 atmospheres, the curves for ether, alcohol, thymol, diphenylamine, and toluidine, are so nearly linear that they may be accepted as such with an error no larger than 2 or 3 degrees at 1000 atmospheres." He also found that in the case of water the rectilinear relation does not hold.

If an isochoric diagram be constructed from the results given on p. 116, it will be seen that, except at small volumes, the isochoric lines are approximately straight, but curve considerably on approaching the condensation points. The lines should probably, as Barus found, be curved throughout, but no considerable error is introduced in considering them as straight during the major part of their course. Indeed, accepting REGNAULT'S determinations as correct, it would appear that at temperatures above 140°, the curvature cannot be due to premature condensation, since the isothermal curves given in the diagram have been drawn, as already stated, to coincide with the results of Regnault's work on the heats of vaporization, and yet coincide with our experimental results, except at volumes very close to those at which liquefaction takes place; and at such small volumes, surface condensation is unmistakeable.

On reference to the Appendix, p. 128, an account of experiments at much lower

temperatures will be found. These show that the relative effect of surface condensation is much more marked at low than at high temperatures. Thus, at about 30 millims. pressure the vapour-density calculated at 75° is 9.01; at 50°, 9.46; at 40°, 9.90; and at 30°, 10.70. An increase of pressure does not appear to raise the apparent vapourdensity to the same extent as a fall of temperature. This may explain why an increase of pressure, at high temperatures, does not influence surface condensation appreciably, except very close to the point of condensation.

In addition to the work of REGNAULT, that of FAIRBAIRN and TATE on the densities of unsaturated and saturated steam may be mentioned. As their results were given in English units, we think it well to reproduce them here in the same form as has been adopted in this paper. It will be seen that the densities of the saturated vapour show a gradual rise with increase of temperature, although the results of individual experiments are far from regular.

FAIRBAIRN and TATE, 'Phil. Trans.,' 1860, pp. 218, 219. Quoted by RANKINE in Fahr. degrees and cubic feet per lb.

T. ° C.	T. ° Abs.	Volume of 1 grm.	Pressure.	Vapour-density.
	7.7.00	c.cs.	millims.	
58.20	331.20	8275.3	135.9	9.15
68.51	341.51	5333.5	218.9	9.09
70.75	343.75	4920.2	240.0	9.05
77.18	350.18	3722.6	316.7	9.23
77.49	350.49	3715·1	320.3	9.15
79.40	352.40	$3438 \cdot 1$	346.0	9.21
83.50	356.50	3051.0	406.7	8.93
86.83	359.83	$2623 \cdot 4$	466.4	9.14
92.65	365.65	2149.5	$581 \cdot 1$	9.10
117.16	390.16	943.12	1361.7	9.44
118.23	391.23	908.03	1410.1	9.49
118.45	391.45	892.54	1419.6	9.60
124.16	397:16	759.44	1697.7	9.57
128.41	401.41	649.24	1935.4	9.93
130.67	403.67	635.30	2070.8	9.54
131.77	404.77	605.65	2138.9	9.71
134.86	407.86	584.44	2342.6	9.26
134.05	407.05	543.17	2287.9	10.18
137.45	410.45	514.98	2529.8	9.79
139.21	412.21	497.25	$2655 \cdot 2$	9.70
141.80	414.80	458:30	2864.6	9.82
144.74	417.74	433.12	3105.1	9.65
142.36	415.36	449.62	2901.9	9.89

THE PROPERTIES OF WATER AND OF STEAM.

'Edinb. Trans.,' vol. 23, 1862, p. 147. FAIRBAIRN and TATE. Superheated Steam. Results arranged in isotherms, and Pressures and V.D.'s corrected for vapour pressure of mercury, using (1) Pressures used by Rankine, (2) Pressures by Ramsay and Young.

Tempera- ture.	Tempera- ture.	Weight.	Volume.	P ₁ .	P_2 .	V. D. (1.)	V. D. (2.)
° F.	° C.	grms.	c.cs.	millims.	millims.	AND THE CONTROL OF STREET STREET, STREET STREET, STREET STREET, STREET	
302.88	150.5	0.01845	197.3	132 3	134.0	9.31	9.19
,,	,,	0.02625	197.3	184.6	186.3	9.48	9.39
,,	,,	0.03530	197.3	250.4	252.1	9.41	9.34
-,,	,,	0.03435	197.3	242.0	243.7	9.46	9.40
	1	0.05670	197.3	408.6	410.3	9.25	9.22
$25\overset{,,}{1.}64$	122.0	0.01845	197.2	123.8	124.7	9.29	9.22
"	,,	0.02625	197.2	171.5	$172 \cdot 4$	9.53	948
"	,,	0.03530	197.2	234.0	234.9	9.39	9.36
"	22	0.03435	197.2	226.1	227.0	9.46	9.42
	,,	0.05670	197.2	381.6	382.5	9.25	9.23
200.74	93.75	0.01845	197.1	114.7	115.1	9.31	9.28
,,	,,	0.02625	197.1	159.9	160.3	9.49	9.47
,,	,,	0.03530	197.1	217.1	217.5	9.41	9.39
"	,,	0.03435	197.1	210.0	210.4	9.46	9.44
	1	0.05670	197.1	$353 \cdot 2$	353.6	9.28	9.27
180.72	82.6	0.04670	197.0	340.2	340.5	9.35	9.34
165.45	74.15	0.03435	197.0	197.3	197.5	9.53	9.52
••	,,	0.05670	197.0	259.3	259.5	11.98	11.97
1 50.18	65.65	0.01845	196.9	105.7	105.9	9.34	9.32
,,	,,	0.02625	196.9	147.6	147.8	9.50	9.49
"	,,	0.03530	196.9	176.1	176.3	10.72	10.71
"	1	0.03435	196.9	177.1	177.3	10.37	10.35
100°0	37.75	0.01845	196.8	44.6	44.7	20.3	20.3

Hirn, in his 'Théorie Mécanique de la Chaleur,' vol. 1, 3rd Ed., p. 468, gives a table of the densities of saturated vapour at various temperatures, ranging from 98° As these agree absolutely with the results calculated from REGNAULT'S measurements, and as neither the method adopted by Hirn, nor his individual observations would appear to lead one to anticipate such concordance, we would suggest that it may be attributed to the "tracé de sentiment" with which he credits the assistant who interpreted his results.

In conclusion, it may be noted that REGNAULT made experiments on the densities of saturated steam at low temperatures for hygrometric purposes, and has shown that it is practically normal at temperatures between 0° and 27° ('Annales de Chimie' [3], vol. 15, 1845, p. 129, et seq.).

Note.—In Plate 7 the curves representing the relations of temperature, pressure, and volume of unsaturated and saturated steam are given on a scale large enough, we hope, to prove of practical use. For this purpose they have been divided into three sets, a different scale, however, being applied to each set. The pressures are given in metres of mercury; the volumes, in cubic centimetres per gramme. The heavy line shows the volumes of saturated vapour, and may be termed the orthobaric line.

DRS. W. RAMSAY AND S. YOUNG ON SOME OF

APPENDIX.

Volumes (Vapour pressures) and Compressibility of Liquid Water at various Temperatures.

Tempera- ture.	Divisions of tube.	Pressure.	Actual volumes.	Tempera- ture.	Divisions of tube.	Pressure.	Actual volumes.
0		millims.	cub. centims.	O		millims.	cub. centims.
100	256.85	760	1.1503	210	288.00	17,488	1.2937
,,	256.50	19,651	1.1488	,,	287.50	31,467	1.2912
110	258.80	1,073	1.1546	,,	287.00	43,405	1.2888
120	260.95	1,484	1.1682	220	$292 \cdot 30$	17,622	1.3138
130	263.10	2,019	1.1775	,,	292.00	$27,\!251$	1.3128
140	265.70	2,694	1.1900	12	291.50	39,432	1.3105
150	268.25	3,568	1.1998	230	297.00	21,085	1.3367
160	271.05	4,652	1.2126	,,	296.50	31,745	1.3343
170	274.00	5,937	1.2267	71	296.00	42,249	1.3319
180	277.10	7,478	1.2416	240	302.00	$25,\!276$	1.3584
190	280.60	9,837	1.2583	22	301.50	$32,\!452$	1.3563
,,	280.50	12,813	1.2579	,,	301.00	41,614	1.3543
,,	280.00	30,029	1.2555	250	307:20	30,059	1.3801
,,	279.50	39,904	1.2532	,,	307.00	36,040	1.3793
200	284.20	15,014	1.2755	,,	306.50	43,925	1.3773
"	284.00	18,695	1.2746	260	313.40	35,028	1.4059
,,	283.50	30,513	1.2723	1,	313.00	40,210	1.4043
"	283.00	43,901	1.2698	270	319.50	43,433	1.4334
210	288.05	14,404	1.2942			,	

Vapour-pressures of Water.—Individual Observations.

Temperature.	Pressure.	Mean corrected.*	Pressure.†	Temperature.	Pressure.	Mean corrected.*	Pressure.†
120	$\begin{array}{c} \text{millims.} \\ 1,482 \end{array}$	millims.	millims.	° 140	millims. 2,691	millims.	millims.
	1,484 1,483 1,493 1,483	1,484	1,445		2,701 2,703 2,695 2,700	2,694	2,658
130	2,024 2,022 2,021 2,018 2,022	2,019	1,950	$150 \ (\mathrm{Jacket} \ \mathrm{C_6H_5~Br})$	3,555 3,552 3,559 3,558 3,569	3,553	3,475

^{*} For deviation from Boyle's law, and for vapour-pressure of mercury. In previous work the measurements of pressure were made rapidly; after the volume had been increased to its maximum, it was diminished by stages, and pressure was read at each stage. The correction for vapour-pressure of mercury is in such a case not admissible. But in this research the temperature was allowed to remain constant for at least an hour before taking the first reading.

[†] Observed with a much smaller quantity of liquid present—nearly all vapour.

THE PROPERTIES OF WATER AND OF STEAM. 121 Vapour-pressures of Water.—Individual Observations—(continued).

Temperature.	Pressure.	Mean corrected.	Pressure.	Temperature.	Pressure.	Mean corrected.	Pressure
$150 \atop (\mathrm{Jacket} \atop \mathrm{C_6H_5NH_2})$	millims. 3,580 3,580 3,588 3,590 3,594	millims.	millims.	210	millims. 14,338 14,329 14,320 14,343 14,383	millims.	millims.
160	4,656 4,648 4,660 4,668 4,671	4,652	4, 609	210	14,337 14,346 14,342 14,382 14,377	14,255	
170	5,958 5,958 5,939 5,966	5,937	5,889	210	$14,324 \\ 14,321 \\ 14,326$	14,223	
180	5,966 7,549			220	17,484 17,468 17,490	17,329	$\left\{ \begin{array}{l} 17,472* \\ 17,426 \end{array} \right.$
(Aniline)	7,559 7,547 7,552 7,581 7,536 7,519	7, 518 ·	7,493	(End of work)	17,498 17,519 17,541 17,582 17,632	17,401	
180	7,480 7,539 7,578 7,423			230	21,059 21,175 21,163 21,158 21,152	20,936	20,879
(Methyl Sali- cylate)	7,453 7,446 7,449 7,467 7,457 7,457	7,437		240	25,296 25,294 25,340 25,399 25,393	25,019	$\left\{egin{array}{l} 24,803* \ 25,040 \end{array} ight.$
190	7,452 7,474 9,425 9,418			250	30,150 30,130 30,142 30,214 30,272	29,734	{ 29,527* { 29,687
	9,431 9,425 9,456 9,469 9,484 9,462	9,403	9,374	260	35,644 35,630 35,649 35,654 35,650	35,059	35,036
200	11,679 11,685 11,674 11,708 11,705	11,625	11,564	270	41,913 41,890 41,869 41,864 41,861 41,821	41,101	$egin{cases} 40,956* \ 41,149 \end{cases}$

^{*} Determinations with two separate quantities, one of which was larger than the other.

DRS. W. RAMSAY AND S. YOUNG ON SOME OF

Volumes of 1 grm. of Steam, at Various Temperatures and Pressures.

I. High Temperatures.

Two series of experiments were made. The weight of the water in the tube was ascertained by determining the products of pressure and volume, altering the volumes; and this was repeated at different temperatures. Assuming that if these products for any one temperature were constant, the density of the steam was constant, viz., the theoretical density, 9, the weight could be ascertained by the equation

$$W = \frac{V.D. \times p.v \times 273}{11.1636 \times 1000 \times 760 \times (273 + t)}.$$

This expression simplifies to

$$\log W = \log p.v. + \overline{4}.46179 - \log (273 + t).$$

During the progress of the experiments it happened that a trace of water passed up the tube, adding itself to that already present. This, of course, increased the weight, hence new measurements were made to determine the amount of the increase.

These weights were obtained from the following readings:—

Determination of the Weight of the Smallest Quantity of Water.

Temperature.	Volume.	Pressure.	p. v.	Weight.	Mean weight
0	cub. centims.	millims.		grm.	grm.
220	1.7147	2528	4335	0.002546	
	1.5565	2770	4311	0.002533	
	1.4080	3060	4308	0.002531	
	1.2592	3435	4325	0.002541	
	1.1072	3893	4310	0.002532	0.002536
230	1.7151	2585	4434	0.002553	
	1.5569	2820	4391	0.002529	
	1.4084	3119	4393	0.002529	
	1.1579	3815	4417	0.002543	0.002538
	Нака пота ж	otor roso in the	o tubo and inc	roseed the weight	
	Here some w	ater rose in the	e tube and inc	reased the weight	
230	1.7151	2633	4516	0.002600	
230		2633 2879	$\begin{array}{c} 4516 \\ 4482 \end{array}$	0·002600 0·002581	
2 30	1.7151	2633	4516	0.002600	0·002579
230 240	1·7151 1·5569	2633 2879	$\begin{array}{c} 4516 \\ 4482 \end{array}$	0·002600 0·002581	
	1·7151 1·5569 1·4084	2633 2879 3153	4516 4482 4441	0.002600 0.002581 0.002587	
	1·7151 1·5569 1·4084 1·7156	2633 2879 3153 2697	$4516 \\ 4482 \\ 4441 \\ 4627$	0.002600 0.002581 0.002587 0.002612	0.002579
	1·7151 1·5569 1·4084 1·7156 1·5573	2633 2879 3153 2697 2948	$4516 \\ 4482 \\ 4441 \\ 4627 \\ 4591$	0.002600 0.002581 0.002587 0.002612 0.002598	
	1·7151 1·5569 1·4084 1·7156 1·5573 1·4087 1·1582 1·5064	2633 2879 3153 2697 2948 3253 3964 3097	4516 4482 4441 4627 4591 4583 4591	0.002600 0.002581 0.002587 0.002612 0.002598 0.002587 0.002592	0.002579
240	1·7151 1·5569 1·4084 1·7156 1·5573 1·4087 1·1582 1·5064 1·4091	2633 2879 3153 2697 2948 3253 3964 3097 3310	4516 4482 4441 4627 4591 4583 4591 4665 4664	0.002600 0.002581 0.002587 0.002612 0.002598 0.002587 0.002592 0.002582 0.002581	0·002579 0·002597
240	1·7151 1·5569 1·4084 1·7156 1·5573 1·4087 1·1582 1·5064	2633 2879 3153 2697 2948 3253 3964 3097	4516 4482 4441 4627 4591 4583 4591	0.002600 0.002581 0.002587 0.002612 0.002598 0.002587 0.002592	0.002579

THE PROPERTIES OF WATER AND OF STEAM.

DETERMINATION of the Weight of the Smallest Quantity of Water. (A.)—(continued).

Temperature.	Volume.	Pressure.	p. v.	Weight.	Mean weight.
	Here more wa	nter rose in the	tube and incr	eased the weight.	3
250	cub. centims. 1.7160 1.5577	millims. 2819 3114	4837 4851	grms. 0·002679 0·002686	grm.
	1·4091 1·1585	3403 4155	4795 4813	$0.002655 \\ 0.002665$	0.002671
260	1·7165 1·5580 1·4094	2872 3144 3478	4930 4899 4902	0.002678 0.002662 0.002663	
970	1.7160	4220	4890	0.002657	0.002665
270	$1.7169 \\ 1.5585 \\ 1.4099 \\ 1.1591$	2918 3196 3529 4283	5010 4981 4975 4964	0.002672 0.002657 0.002654 0.002648	0.002656
'	2 3002		ean, 0.002664.	OCOMORO	1 0002000

These results can be verified by taking the weight at 270° as a standard, and calculating the smaller weights by the equation

$$\frac{p.v.}{273+t}:\frac{p'v'}{273+t'}::W:W'$$

identical numbers with those found are obtained.

Hence the largest weight at 250°, 260°, and 270° is 0.002664 grm.; the second weight at 250° , 240° , and 230° is 0.002588 grm.; the first weight at 220° and 230° is 0.002547 grm.

The first weight holds also for lower temperatures.

These data are adduced as a proof of the relative accuracy of the determinations which follow.

DRS. W. RAMSAY AND S. YOUNG ON SOME OF

Volumes of 1 grm. of Steam and Vapour-densities.

Temperature.	Pressure.	Volume of 1 grm.	p. v.	$\begin{array}{l} \text{Vapour-} \\ \text{density} \\ \text{H} = 1. \end{array}$	Remarks.
120	millims. 1,448 1,450	c.c. 602·0 545·2	• •	• •	Condensed Condensed
130	1,930 1,953	622·7 563·7	• •	• •	Condensed Condensed
140	2,093 2,245 2,449 2,620 2,645 2,650	661·7 609·9 551·7 453·6 338·3 107·1	1,384,900 1,369,200 1,351,100 1,188,400 894,810	9·268 9·374 9·500 10·800	Condensed Condensed
150	2,147 2,309 2,550 3,068 3,280 3,442 3,475	661·8 610·0 551·8 453·7 415·2 353·9 241·5	1,420,900 1,408,500 1,407,100 1,392,000 1,361,900	9·251 9·333 9·343 9·445 9·654	Condensed Condensed
150	$2{,}149$ $2{,}310$ $2{,}547$	661.8 610.0 551.8	1,422,200 1,409,100 1,405,400	9·243 9·329 9·354	
160	2,211 2,382 2,633 3,182 3,997 4,571	662.0 610.2 552.0 453.8 354.1 241.6	1,463,700 1,453,500 1,453,400 1,444,000 1,415,300	9·193 9·258 9·259 ? 9·319 9·509	Condensed
170	2,267 2,447 2,705 3,271 4,172 5,603	662·2 610·3 552·1 453·9 354·1 252·7	1,501,200 1,493,400 1,493,500 1,484,700 1,477,300 1,415,900	9.171 9.219 9.219 9.273 9.364 9.722	
180	2,330 2,509 2,771 3,356 4,271 5,854 7,296 7,444 7,471	$662\cdot 4$ $610\cdot 5$ $552\cdot 2$ $454\cdot 0$ $354\cdot 2$ $252\cdot 8$ $192\cdot 5$ $152\cdot 3$ $112\cdot 1$	1,543,400 1,531,800 1,530,100 1,523,600 1,512,800 1,479,900. 1,404,500	9·122 9·193 9·200 9·240 9·306 9·512 10·025	Condensed Condensed
190	2,387 2,576 2,842 3,441 4,385	662·6 610·7 552·4 454·2 354·3	1,581,600 1,573,200 1,569,900 1,562,900 1,553,600	9.098 9.147 9.172 9.208 9.261	

THE PROPERTIES OF WATER AND OF STEAM.

Volumes of 1 grm. of Steam and Vapour-densities—(continued).

Temperature.	Pressure.	Volume of 1 grm.	p. v.	Vapour density H = 1.	Remarks.
190 (continued)	millims. 6,057 7,839 9,254 9,337	c.c. 252·9 192·5 152·3 112·2	1,531,800 1,509,000 1,409,400	9·393 9·534 10·207	Condensed
200	2,458 2,655 2,930 3,546 4,516 6,276 8,107 10,004 11,505	$\begin{array}{c} 662.7 \\ 610.8 \\ 552.5 \\ 454.2 \\ 354.4 \\ 253.0 \\ 192.6 \\ 152.4 \\ 112.2 \end{array}$	1,628,900 1,621,700 1,618,800 1,610,600 1,600,400 1,587,800 1,561,400 1,524,600	9·024 9·065 9·080 9·126 9·185 9·260 9·738 10·246	$\mathbf{Condensed}$
210	2,525 2,723 3,000 3,652 4,646 6,437 8,371 10,331 13,538 14,102	662·9 611·0 552·7 454·4 354·5 253·1 192·6 152·4 112·2 92·2	1,673,300 1,663,800 1,658,100 1,659,500 1,647,000 1,629,200 1,612,300 1,574,400 1,519,000 1,300,200	8·989 9·023 9·053 9·048 9·114 9·214 9·309 9·533 9·880 11·548	
220	2,585 2,782 3,072 3,734 4,758 6,601 8,580 10,649 14,073 16,458 17,165	663·0 611·1 552·8 454·5 354·6 253·1 192·7 152·4 112·2 92·2 72·2	1,713,800 1,700,100 1,698,200 1,697,100 1,687,300 1,670,700 1,653,400 1,622,900 1,579,000	8·939 9·012 9·022 9·029 9·082 9·171 9·268 9·438 9·699 10·098	$\mathbf{Condensed}$
220	2,529 2,770 3,060 3,435 3,894 4,493 5,685 7,114 8,575 10,638 14,032 16,641 17,476	675·9 613·5 555·0 496·3 436·4 376·2 294·3 235·8 193·4 153·0 112·7 92·6 72·5	1,709,400 1,699,400 1,698,300 1,704,800 1,699,400 1,690,300 1,673,100 1,677,500 1,658,400 1,627,600 1,581,400 1,541,000 1,267,000	8.964 9.016 9.022 8.986 9.016 9.064 9.136 9.134 9.237 9.411 9.690 9.948 10.059	Weight altered
230	2,585 2,820	676·1 613·7	1,747,700 1,730,700	8·945 9·033	

DRS. W. RAMSAY AND S. YOUNG ON SOME OF Volumes of 1 grm. of Steam and Vapour-densities—(continued).

Temperature.	Pressure.	Volume of 1 grm.	р. v.	Vapour- density H = 1.	Remarks.
230 (continued)	millims. 3,119 3,615 4,840 6,725 8,815 10,887 14,430 17,148 20,662 20,884	c.c. 555·1 477·9 356·1 254·1 193·5 153·1 115·1 92·6 72·5 52·5	1,731,400 1,727,600 1,723,500 1,708,800 1,705,700 1,666,800 1,660,900 1,587,900 1,498,000	9·028 8·978 9·070 9·146 9·165 9·380 9·633 9·847 10·433	$\mathbf{Condensed}$
230 (repeated)	2,633 2,879 3,153	664·5 603·2 545·7	1,749,600 1,736,600 1,720,600	8·934 9·002 9·086	Taken as normal; weight altered
240	2,697 2,948 3,253 3,964 5,053 7,002 9,158 11,395 15,084 17,998 21,336 22,162 25,049	664.7 603.4 545.8 448.7 350.1 249.9 190.2 150.5 110.8 91.0 71.3 61.4 41.7	1,792,700 1,778,900 1,775,500 1,778,600 1,769,000 1,749,800 1,741,900 1,715,000 1,671,300 1,637,800 1,524,100 1,360,700	8·691 8·973 8·980 8·963 9·012 9·112 9·170 9·151 9·296 9·559 9·732 10·480	Doubtful Condensed
250	3,097 3,310 4,027	583·6 545·9 448·8	1,807,400 1,806,900 1,807,300	8·992 8·995 8·993	
250 (repeated)	2,819 3,114 3,403 4,155 5,290 7,367 9,560 11,907 15,852 18,897 23,594 26,395 29,473 29,696	644·2 584·7 528·9 434·9 339·3 242·2 184·4 145·9 107·4 88·2 69·1 59·5 50·0 31·0	1,816,000 1,820,800 1,799,800 1,807,000 1,794,900 1,784,300 1,762,900 1,737,300 1,702,500 1,666,700 1,630,400 1,570,500 1,473,600	8.951 8.927 9.030 8.996 9.056 9.110 9.222 9.359 9.547 9.751 9.970 10.343 11.034	Condensed
260	2,872 3,144 3,479 4,225 5,409 7,521	644·3 584·9 529·1 435·0 339·4 242·2	1,850,400 1,838,900 1,840,800 1,837,900 1,835,800 1,821,600	8·952 9·008 9·000 9·013 9·045 9·093	

THE PROPERTIES OF WATER AND OF STEAM. Volumes of 1 grm. of Steam and Vapour-densities—(continued).

Temperature.	Pressure.	Volume of 1 grm.	p. v.	Vapour density H = 1.	Remarks.
260 (continued)	millims. 9,811 12,164 16,228 19,326 23,886 27,193 31,142 35,040	c.c. 184·4 145·9 107·4 88·2 69·1 59·6 50·0 31·0	1,809,100 1,774,800 1,741,800 1,704,600 1,650,500 1,620,700 1,571,000	9·177 9·334 9·501 9·714 10·034 10·229 10·640	Condensed
270	2,918 3,196 3,529 4,288 5,486 7,664 9,974 12,392 16,519 19,729 24,427 27,813 31,958	644·5 585·0 529·2 435·1 339·5 242·3 184·4 145·9 107·5 88·3 69·1 59·6 50·0	1,880,700 1,869,700 1,867,600 1,865,700 1,862,600 1,857,000 1,839,200 1,808,000 1,775,800 1,742,100 1,687,900 1,657,700 1,597,900	8·973 9·025 9·036 9·045 9·062 9·088 9·173 9·331 9·507 9·691 9·993 10·185 10·560	
	37,862 $40,854$	40·5 29·1	1,533,400	11.010	Condensed

II. Low Temperatures.

(a.) Weight of water in the modified Hofmann's apparatus (described with a wood-cut in 'Phil. Trans.,' 1887 A., p. 59).

0.20087 grm.

Readings commenced at largest volume, and vapour then compressed.

Tempera-	Pressure.	Volume.	Vapour Density (H = 1).	Tempera- ture.	Pressure.	Volume.	Vapour Density (H = 1).
7 5	millims. 23·35 23·40 23·65 25·80 27·4 29·6 32·2 35·3 39·95 45·7	c.c. 150·5 148·5 146·3 134·9 125·9 116·4 106·2 96·36 86·52 74·78	8·83 8·93 8·97 8·92 8·99 9·01 9·08 9·13 8·98 9·08	40	millims. 19·15 21·2 23·15 26·0 29·2 33·75 39·3 48·45 52·2 54·1	c.c. 149·1 135·7 122·3 109·0 96·54 83·07 71·10 55·90 49·66 42·05	9·78 9·71 9·86 9·85 9·90 9·96 9·99 10·31 10·77 12·27
75 (repeated)	23·6 24·1 30·3 47·65 57·7 79·2	146·9 141·2 111·9 72·17 58·12 42·76	8·96 9·12 9·16 9·03 9·26 9·17	30	18·05 18·9 20·1 22·1 24·45 26·7 29·9 31·05 31·35 31·45	154·9 145·2 134·5 122·0 109·0 96·72 84·50 68·61 55·0 43·0	9·66 9·85 10·00 10·03 10·14 10·46 10·70 (12·69) Condensed
50	20·35 21·8 23·4 26·95 33·25 42·1 54·75 70·75	153·0 140·5 130·5 113·2 91·35 71·82 54·49 42·52	9·25 9·40 9·43 9·45 9·49 9·53 9·66 9·58	25	17·25 18·0 19·25 20·35 21·8 22·4 23·35·	154·2 144·8 134·4 123·1 111·6 99·32 86·5	9·99 10·20 10·27 10·62 10·93 11·95 (13·16)

It is to be noticed that four readings are required for each pressure, so that at the lowest pressure an error of 1 per cent., or say 0.2 millim., is not excessive.

In considering these results it is seen that, as a rule, the density increases on diminishing volume. This, however, cannot be ascribed to real increase of density, but to diminution of the actual weight of the water present in the state of vapour through adhesion of water to the surface of the tube. That this explanation is the correct one is seen from the following considerations.

At 75° very little rise of vapour-density is to be observed, although there is a slight tendency towards a higher value at the smallest volumes. The pressure was never near the vapour-pressure, which at this temperature is 288.5 millims.

THE PROPERTIES OF WATER AND OF STEAM.

At 50°, at which the vapour-pressure is 92 millims, the vapour-densities are all high, but do not rise rapidly after the first one. The highest pressure registered (70.75) approached the vapour-pressure.

At 40° the vapour-pressure is 54.9; the highest pressure read was 54.1. of vapour-density is slow at first, and afterwards more rapid.

At 30° the vapour-pressure is 31.55 millims, while the highest pressure read was 31.05 millims. The vapour-densities are very high, and rise rapidly with decrease of volume; and at 25° the vapour-pressure is 23.55 millims., the highest pressure read being 23:35. Again, there is a rapid increase of density with diminishing volume.

These pressures are all somewhat lower than the values given by REGNAULT.

(b). Weight = 0.00295 grm.

The tube was heated to 100°.

Tempera- ture.	Pressure.	Volume.	Vapour- density.
100	millims. 25·1 28·7 34·1 41·45 52·4	c.c. 152·4 131·3 110·4 91·13 72·34	8·94 9·08 9·08 9·05 9·02

The tube was then cooled with the mercury at the same height as at the last reading, and then, without drawing down the mercury, the tube was heated to 40°. In this case there was no possibility of condensation of vapour on the lower part of the tube, while previously, when readings were begun at the largest volume, condensation might have taken place on the lower part of the tube. If, therefore, the high vapour-densities are due to adhesion and condensation, the value of this reading at 40° should be lower than it was found in the first series. This is in fact the case, as is shown by the following determinations:—

Tempera- ture.	Pressure.	Volume.	Vapour- density.
° 40	millims. 42·05 45·75 51·6 53·95 54·8	c.e. 71·7 64·63 55·41 49·83 42·0	9·52 9·70 10·04 10·67 Condensed.

In the first series, at volume 71.1 cub. centims., the vapour density was 9.99, as against 9.52 in the second at volume 71.7 cub. centims. The largest volume in the MDCCCXCII.—A.

first series, 149.1, is a little more than twice as great as the largest volume in the second; therefore, as the tube was cylindrical, the surface on which condensation could take place was about twice as great. If the condensation is not much affected by the rise of pressure from 19.15 millims, at the largest volume of the first series to 42.05 millims at the largest volume of the second, and if the high vapour-density is entirely due to condensation, we should expect the error to be about half as great in the second as in the first series, and this is approximately the case. noticed that the weight of the water in both sets is nearly the same.

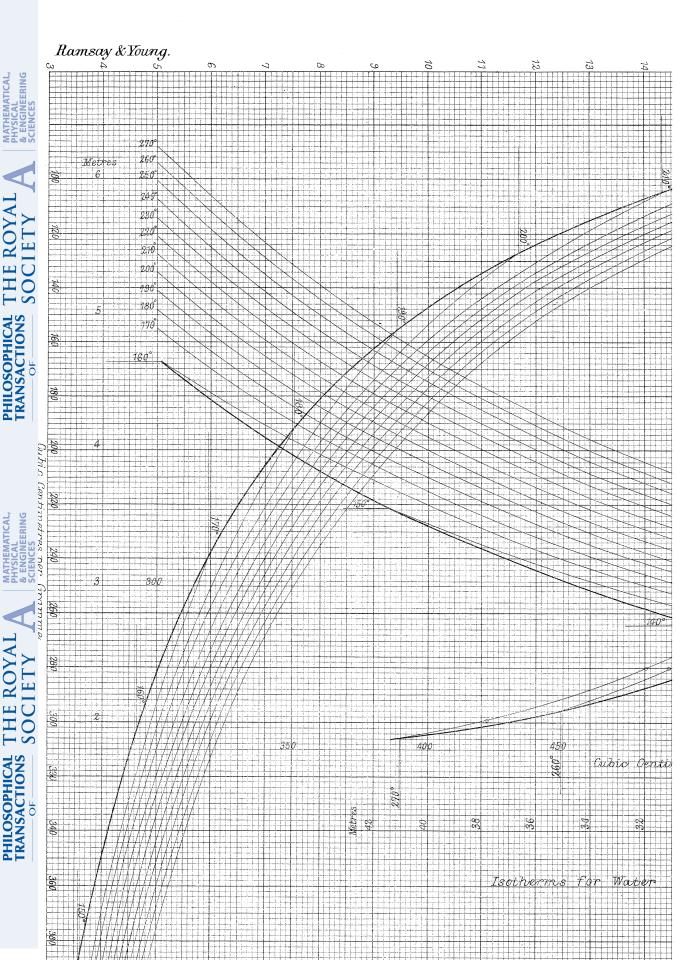
The tube was again heated to 100°, and the external pressure so arranged that the volume of vapour remained about 56 cub. centims. After cooling, the tube was again heated to 40°, and a reading was taken with the following results:—

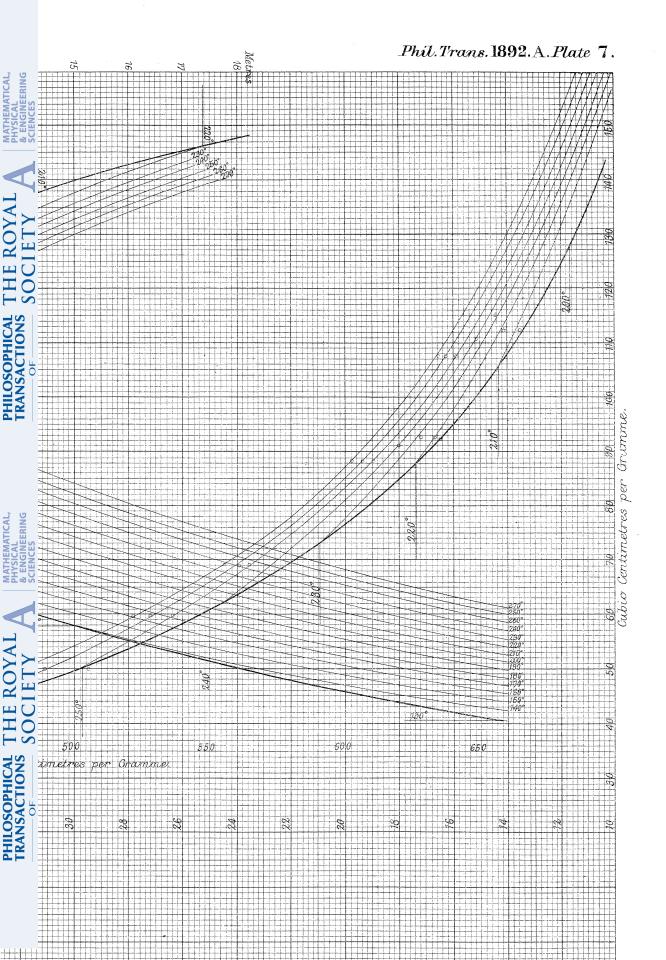
Tempera- ture.	Pressure.	Volume.	Vapour- density.
° 40	$rac{ ext{millims.}}{52 \cdot 3}$	c.c. 54·87	10.00

The result is not much lower than at the corresponding volume in the last experiment, but the gain of surface was not very great, and the pressure, 52.3 millims., was very near the condensing pressure, 54.9 millims.; and it is to be noticed that the vapour-density rises rapidly as this pressure is approached. At the same pressure in the first series, the vapour-density observed was 10.77—a much higher value,

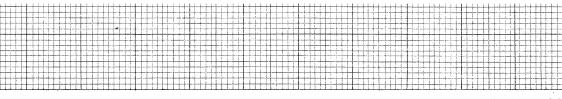
The experiments show that the high vapour-densities are due to condensation on the walls of the tube, and that the error due to this cause may vary considerably, especially at pressures near the true vapour pressures.

Similar experiments were not made at high pressures, but on constructing isothermal curves, it is seen that as the volume diminishes, and as the vapour-pressure is approached, the curves instead of cutting the vapour-pressure line so as to form an angle, as is the case with the other liquids which we have examined, gradually turn and run nearly parallel to the vapour-pressure line at a somewhat lower pressure. When a considerable amount of liquid has condensed, the true vapour-pressure is This behaviour is analogous to that of a mixture of a condensible vapour with a gas like air; but it cannot be attributed to such admixture, for the last bubble of steam left on raising pressure was easily and quickly absorbed, and without any perceptible rise of pressure. Its cause must, as already explained, lie in the adhesion of the vapour to the glass, causing condensation before the true vapourpressure is reached.





3600



West, Newman lith.

